U.S. DEPARTMENT OF COMMERCE, PATENT AND TRADEMARK OFFICE

### TRANSMITTAL LETTER TO THE UNITED STATES DESIGNATED/ELECTED OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. 371

ATTORNEY'S DOCKET NUMBER

33808F147

U.S. APPLICATION NO. (if known,

INTERNATIONAL APPLICATION NO. INTERNATIONAL FILING DATE PRIORITY DATE CLAIMED PCT/FR99/02744 9 November 1999 13 November 1998 TITLE OF INVENTION POLYMERS FLUORINATED BY POLYMERISATION IN MINI-EMULSION APPLICANT(S) FOR DO/EQ/US Dennis Tembou Nzudie, et al.

Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:

- This is a FIRST submission of items concerning a filing under 35 U.S.C. 371.
- 2. This is a SECOND or SUBSEQUENT submission of items concerning a filing under 35 U.S.C. 371.
- This express request to begin national examination procedures (35 U.S.C. 371(f) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U.S.C. 371(b) and PCT Articles 22 and 39(l).
- 4. 

  A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.
- a R is transmitted herewith
  - b. 

    has been transmitted by the International Bureau (see accompanying PCT Form 308).

  - A translation of the International Application into English (35 U.S.C. 371(c)(2)).
- Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3)).
- a. are transmitted herewith (required only if not transmitted by the International Bureau).
- b. I have been transmitted by the International Bureau.
- c. a have not been made; however, the time limit for making such amendments has NOT expired. d. a have not been made and will not be made.
- ☐ A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)).
- An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)).
- ⊕10. □ A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)).

### Hems 11. to 16. below concern other document(s) or information included:

- ♣1. 

  An Information Disclosure Statement under 37 CFR 1.97 and 1.98.
- 2. 

  An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.
  - 13. 

    A FIRST preliminary amendment.
  - □ A SECOND or SUBSEQUENT preliminary amendment.
  - 14. A substitute specification.
  - 15. 

    A change of power of attorney and/or address letter.
- a. PCT Request (PCT/RO/101) (in French)
- b. Notification of Transmittal of the International Preliminary Examination Report (PCT/IPEA/416) (in French);
- c) International Preliminary Examination Report (PCT/IPEA/409) (in French)
- c. International Search Report PCT/ISA/210 (attached to WO 00/29457)(in French)
- e. Applicant's Reply to Written Opinion dated December 15, 2000 (in French)

(Page 2) U.S DEPARTMENT OF COMMERCE, PATENT AND TRADEMARK OFFICE ATTORNEY'S DOCKET NUMBER TRANSMITTAL LETTER TO THE UNITED STATES 33808F147 DESIGNATED/ELECTED OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. 371 U.S. APPLICATION NO. (if known, 99 8 31 575 17. 

The following fees are submitted: CALCULATIONS PTO USE ONLY Basic National Fee (37 CFR 1.492(a)(1)-(5)): International preliminary examination fee paid to USPTO (37 CFR 1.482) ..... No international preliminary examination fee paid to USPTO (37 CFR 1.482) but international Neither international preliminary examination fee (37 CFR 1.482) nor International preliminary examination fee paid to USPTO (37 CFR 1.482) ENTER APPROPRIATE BASIC FEE AMOUNT = \$860.00 Surcharge of \$130.00 for furnishing the oath or declaration later than 

20 

30 months from the earliest claimed priority date (37 CFR 1.495(e)) Claims Number Filed Number Extra Rate Total Claims 8 -20 = x \$18.00 Independent Claims 2-3= x \$80.00 Multiple dependent claim(s) (if applicable) + \$270.00 TOTAL OF ABOVE CALCULATIONS = \$ 860.00 Reduction by ½ for filing by small entity, if applicable. Verified Small Entity statement must also be filed. (Note 37 CFR 1.9, 1.27, 1.28). SUBTOTAL = \$ 860.00 Processing fee of \$130.00 for furnishing the English translation later than 

20 

30 months from the earliest claimed priority date (37 CFR 1.492(f)). TOTAL NATIONAL FEE = 860.00

must be filed and granted to restore the application to pending status.

by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40.00 per property.

b. 

Please charge my Deposit Account No. \_\_\_ \_\_ in the amount of \$\_\_\_ to cover the above fees.

Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied

c. a The Commissioner is hereby authorized to charge any additional fees which may be required, or credit any overpayment to Deposit Account No. 02-4300.

TOTAL FEES ENCLOSED =

NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met

SEND ALL CORRESPONDENCE TO:

SMITH, GAMBRELL & RUSSELL, LLP The Beveridge, DeGrandi, Weilacher & Young Intellectual Property Group 1850 M Street, N.W., Suite 800

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Frederick F. Calvetti REGISTRATION NO.

860.00 Amount to be refunded s charged

Date: May 11 2001

### IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Applicant(s): Dennis Tembou Nzudie, et al.

International PCT Application No.: PCT/FR99/02744

International Filing Date: 9 May 1999

US Serial No.: To Be Assigned

Group Art Unit: To Be Assigned

Filed: : May 11, 2001 (Herewith)

Examiner: To Be Assigned

For

POLYMERS FLUORINATED BY POLYMERISATION IN MINI-EMULSION

### PRELIMINARY AMENDMENT

Assistant Commissioner for Patents Washington, DC 20231

Sir:

Prior to or concurrent with calculation of the filing fees, please amend this application as follows.

### IN THE SPECIFICATION:

On page 1, after the title, please add the paragraph heading "Field of the Invention"; On page 1, after the first paragraph, please add the paragraph heading "Background of the Invention";

On page 4, line 3, please add the paragraph heading "Description of the Invention";

On page 10, line 6, please add the paragraph heading "Examples";

On page 19, beginning on line 23, please add the new paragraph.

### IN THE CLAIMS:

Applicants have attached to this Amendment documents entitled "Amended Claims" and 
"'Marked-up' Copy of the Previous Claims". Please replace present claims 1-7 in this 
application with amended claims 1-7 shown in the document entitled "Amended Claims". 
Please add new claim 8 as shown in the document entitled "Amended Claims".

### REMARKS

Entry and consideration of this Preliminary Amendment are respectfully requested prior to or concurrent with calculation of the filing fees. This Preliminary Amendment is being filed to correct improper multiple dependencies. As so amended, the claims are submitted as appearing in proper multiple dependent form. No new matter has been added by this amendment.

Examination on the merits is awaited.

### AUTHORIZATION

No additional fee is believed to be necessary.

The Commissioner is hereby authorized to charge any additional fees, which may be required for this amendment, or credit any overpayment to Deposit Account No. 02-4300, Order No. 33808.147.

In the event that an extension of time is required, or which may be required in addition to that requested in a petition for an extension of time, the Commissioner is requested to grant a petition for that extension of time which is required to make this response timely and is hereby

authorized to charge any fee for such an extension of time or credit any overpayment for an extension of time to Deposit Account No. 02-4300, Order No. 33808.147.

Respectfully submitted,
SMITH GAMB RELI & RUSSP LILLE

By:
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May 11, 2001

### CLAIMS

- 1. (Amended) Process for producing
  fluorinated polymers by miniemulsion polymerization in
  two stages comprising
  - a) emulsification of a mixture of monomers comprising:

from 20 to 99.9% by weight of at least one monomer selected from fluorinated (meth)acrylic

10 monomers (A).

from 0.1 to 15% by weight of at least one monomer selected from acrylamide and its compounds,

including N-methylolacrylamide, and

from 0 to 65% by weight of at least one

15 monomer selected from nonfluorinated acrylic or vinyl
monomers (B),

using energetic emulsifying treatment, including ultrasound, colloid mill or high-pressure homogenizer, and

20 . b) polymerization of the said mixture at a temperature ranging from 20 to 100°C using radical initiators,

the level of organic cosolvent being less than 0.2% by weight of the total weight of the 25 emulsion.

2. (Amended) Process according to Claim 1, wherein the mixture of monomers is stabilized by at least one surfactant selected from the group comprising nonionic, anionic or cationic surfactants, including polyethoxylated sulphosuccinate compounds or quaternary ammonium compounds.

3. (Amended) Process according to Claim 1, wherein the fluorinated monomer A is selected from the 5 group comprising the monomers corresponding to the following formulae:

10

in which R<sub>P</sub> represents a perfluorinated radical with a linear or branched chain comprising 2 to 20 carbon atoms, p and q, which are identical or different, each represent an integer ranging from 1 to 20, R<sub>1</sub> represents a linear or branched alkyl radical comprising from 1 to 4 carbon atoms and R<sub>2</sub> represents a hydrogen atom or a methyl radical.

- (Amended) Process according to claim 1, wherein the monomer B is selected from the group
   comprising:
  - $C_1$ - $C_{22}$  alkyl (meth)acrylates
  - (meth)acrylates, the radical of which carries an oxyethylenated linkage

- vinyl monomers, including vinyl chloride or vinyl acetate
  - acrylic and methacrylic acids.
  - 5. (Amended) Process according to claim 1,
- 5 wherein the initiator is selected from the group comprising:
  - peroxides
  - persalts, including persulphates
  - azo compounds, such as 4,4'-azobis
- 10 (4-cyanopentanoic acid).
- 6. (Amended) Aqueous dispersion comprising fluorinated polymers obtained according to the process of claim 1, the content of organic cosolvent of which is less than 0.2% by weight of the total weight of the emulsion and the level of coagulum being less than 1% by weight of the total weight of monomers.
- (Amended) Hydrophobic and oleophobic treatment of substrates comprising treatment of, leather, textiles, fitted carpets, paper and
   construction materials with an aqueous dispersion of the polymer of claim 6.
  - 8. (New) Process according to claim 3, wherein the integer is from 1 to 4.

MARKED UP COPY OF THE PREVIOUS CLAIMS

## JC08 Rec'd PCT/PTO 1 1 MAY 2001

### CLAIMS

- Process for producing fluorinated
   polymers by miniemulsion polymerization in two stages
   comprising
  - a) [the] emulsification of a mixture of monomers comprising:

from 20 to 99.9% by weight of at least one monomer [chosen] selected from fluorinated

10 (meth)acrylic monomers (A),

from 0.1 to 15% by weight of at least one monomer [chosen] selected from acrylamide and its [derivatives] compounds, including [such as] N-methylolacrylamide, and

from 0 to 65% by weight of at least one monomer [chosen] selected from nonfluorinated acrylic or vinyl monomers (B),

using energetic emulsifying [means]

<u>treatment</u>,[such as] <u>including</u> ultrasound, colloid mill

20 or high-pressure homogenizer, and

b) [the] polymerization of the said mixture at a temperature ranging from 20 to  $100\,^{\circ}\text{C}$  using radical initiators,

the level of organic cosolvent being less
25 than 0.2% by weight of the total weight of the
emulsion.

2. Process according to Claim 1, wherein [characterized in that] the mixture of monomers is stabilized by at least one surfactant [chosen] selected

10

from the group comprising nonionic, anionic or cationic surfactants, [such as] <u>including</u> polyethoxylated sulphosuccinate [derivatives] <u>compounds</u> or quaternary ammonium [derivatives] <u>compounds</u>.

3. Process according to Claim 1 [or 2], [characterized in that] wherein the fluorinated monomer A is [chosen] selected from the group comprising the monomers corresponding to the following formulae:

in which R<sub>P</sub> represents a perfluorinated radical with a linear or branched chain comprising 2 to 20 carbon

15 atoms, p and q, which are identical or different, each represent an integer ranging from 1 to 20 [and preferably from 1 to 4], R<sub>1</sub> represents a linear or branched alkyl radical comprising from 1 to 4 carbon atoms and R<sub>2</sub> represents a hydrogen atom or a methyl

20 radical.

4. Process according to [one of the preceding claims] <a href="claim 1">claim 1</a>, [characterized in that] <a href="wherein">wherein</a> the monomer B is [chosen] <a href="selected">selected</a> from the group comprising:

- C1-C22 alkyl (meth)acrylates
- (meth) acrylates, the radical of which carries an oxyethylenated linkage
- vinyl monomers, [such as] including vinyl 5 chloride or vinyl acetate
  - acrylic and methacrylic acids.
- Process according to [one of the preceding claims] claim 1, [characterized in that] wherein the initiator is [chosen] selected from the 10 group comprising:
  - peroxides
  - persalts, [such as] including persulphates
  - azo compounds, such as 4,4'-azobis (4-cyanopentanoic acid).
- Aqueous dispersion [of] comprising fluorinated polymers [as may be] obtained according to the process of [any one of the preceding claims] claim 1, the content of organic cosolvent of which is less than 0.2% by weight of the total weight of the emulsion 20 and the level of coagulum being less than 1% by weight of the total weight of monomers.
- 7. [Application of the aqueous dispersion of Claim 6 in the] [h] Hydrophobic and oleophobic treatment of [various] substrates comprising treatment 25 of, [such as] leather, textiles, fitted carpets, paper and construction materials with an aqueous dispersion of the polymer of claim 6.

- vinyl monomers, including vinyl chloride or vinyl acetate
  - acrylic and methacrylic acids.
  - 5. (Amended) Process according to claim 1,
- 5 wherein the initiator is selected from the group comprising:
  - peroxides
  - persalts, including persulphates
  - azo compounds, such as 4,4'-azobis
- 10 (4-cyanopentanoic acid).
- 6. (Amended) Aqueous dispersion of fluorinated polymers obtained according to the process of claim 1, the content of organic cosolvent of which is less than 0.2% by weight of the total weight of the emulsion and the level of coagulum being less than 1% by weight of the total weight of monomers.
- (Amended) Hydrophobic and oleophobic treatment of substrates comprising treatment of, leather, textiles, fitted carpets, paper and
   construction materials with an aqueous dispersion of the polymer of claim 6.
  - 8. (New) Process according to claim 3, wherein the integer is from 1 to 4.

8. (New) Process according to claim 3, wherein the integer is from 1 to 4.



# 1 FLUORINATED POLYMERS BY MINIEMULSION POLYMERIZATION

The invention relates to the field of aqueous emulsions and in particular to a process for the 5 preparation of aqueous emulsions of fluorinated polymers.

Fluorinated copolymers are used in various applications, in particular in the hydrophobic and oleophobic treatment of various substrates, such as 10 textiles, leather or paper. These fluorinated copolymers are generally prepared by copolymerization in an organic solvent or according to the aqueous emulsion polymerization technique. For reasons of environmental constraints, they are generally prepared 15 by aqueous emulsion copolymerization. For hydrophobic and oleophobic coating applications, these copolymers are obtained from at least one perfluorinated acrylic monomer and at least one nonfluorinated monomer. generally an alkyl acrylate or methacrylate.

The copolymerization of perfluorinated monomers according to the conventional emulsion technique is a technically difficult problem. This is because the strong hydrophobicity of these monomers greatly decreases, on the one hand, the contribution of 25 the initiation of the polymerization in the aqueous phase and, on the other hand, the diffusion of these monomers from the storage drops to the growing

particles. As a result of these particular properties of perfluorinated acrylic monomers, the use of a water-soluble organic solvent is necessary when they are employed in producing an aqueous emulsion. This solvent has to be a good solvent for monomers and must not cause the polymer formed to precipitate, as is the case with certain alcohols.

The most widely used solvent is acetone (see, for example, Patents FR 1,532,053 or FR 2,202,515).

10 However, safety and transportation constraints are prompting a large number of producers to market products without a flashpoint. It is obviously possible, if the surface-active formulation has been carefully selected, to distil off the solvent used in the copolymerization.

However, this decreases the productivity and results in an additional cost with regard to energy consumption, on the one hand, and confers poor stability over time on the emulsion, on the other hand.

20 The use of nonflammable solvents, such as ethylene glycol, propylene glycol and their derivatives, is disclosed in Patent FR 2,175,332 but these compounds generally exhibit a poor solvating power and must be used in combination with acetone. In 25 some commercial fluorinated emulsions, acetone has been replaced by excellent solvents with a high flashpoint, such as N-methylpyrrolidone or y-butyrolactone. The use

of heavy diols, such as dipropylene glycol,
pentanediol, hexanediol and tripropylene glycol, in
producing fluorinated acrylic emulsions without a
flashpoint is disclosed in Patent JP 60.40182. However,
it turns out that such emulsions exhibit a number of

it turns out that such emulsions exhibit a number of drawbacks related to the low volatility of the solvents, such as:

difficult drying of textile and leather articles, which it is impossible to bring to high 10 temperature, and/or

the lack of crosslinking of the copolymer on textiles, due to the incomplete drying of the solvent and to the presence of residual hydroxyl groups.

Whatever the solutions introduced by persons

15 skilled in the art in terms of choice of solvent, it
transpires that problems arise:

- of volatile organic compounds, resulting in pollution, safety and transportation risks if the solvent cannot be distilled off,
- 20 of productivity and of an additional cost with regard to energy consumption, if the formulation comprises a solvent of low boiling point which is distilled off at the end of polymerization.

Furthermore, the conventional emulsion

25 presents a problem of stability and of yield insofar as
emulsion polymerization results in the formation of a

high level of coagulum (1-8%), which coagulum has to be destroyed.

According to the invention, the term
"coagulum" is understood to mean the polymer in the

5 form of a flock which is not stabilized and which
sediments in the polymerization reactor, in contrast to
the polymer present in the latex particle, which
polymer is stabilized in a colloidal fashion by
surfactants.

The problem which the invention seeks to solve is the development of an aqueous emulsion of fluorinated polymers which does not comprise volatile organic compounds, which is stable and which is devoid of coagulum, while observing industrial requirements such as economy in energy and productivity.

The solution has been found by virtue of a specific combination comprising

- the use of a process known as the miniemulsion polymerization process, without the use of organic cosolvent, and
  - the judicious choice of a mixture of monomers necessarily comprising acrylamide or one of its derivatives.

The process is based on a first stage of

25 specific emulsification of the water/monomer/
surfactants mixture using an energetic means, such as
ultrasound, colloid mill or high-pressure homogenizer,

thus generating fine droplets of monomers in the water. The emulsification stage is followed by a polymerization stage.

The process of the invention is distinguished

from conventional processes for the manufacture of
perfluorinated emulsions by, on the one hand, a level
of organic cosolvent in the formulation of less than
0.2% by weight of the emulsion and by, on the other
hand, a level of coagulum of less than 1% by weight of
the total weight of monomers. It thus exhibits the
advantage of being more productive and of generating
little in the way of volatile organic compound, a
source of pollution.

Thus, by using the polymerization technique

known as the miniemulsion polymerization technique,
which technique is known in the literature for the
polymerization of numerous vinyl and acrylic monomers
and in particular an acrylic monomer with a longer or
shorter alkyl chain, perfluorinated acrylic monomers

can be copolymerized with nonfluorinated monomers, with
the following advantages:

 no use of organic cosolvent and therefore fewer volatile organic compounds, no loss in productivity related to distillation and no additional cost with regard to energy consumption,  a higher yield, as coagulum is not formed, even at high levels of incorporation of perfluorinated monomers,

- no use of cosurfactant which is a fatty

5 compound of low solubility in water (hexadecanol,
hexadecane) commonly used in miniemulsions (which can
disturb the final properties).

One of the subject-matters of the invention is a process for producing fluorinated polymers by

10 miniemulsion polymerization comprising the polymerization of a mixture of monomers, which monomers are dispersed in water and which mixture is stabilized by at least one surfactant, characterized in that the level of organic cosolvent in the reaction mixture is

15 less than 0.2% by weight of the total weight of the emulsion.

The term "fluorinated polymers" according to the invention is understood as meaning polymers comprising at least 20% by weight of units derived by polymerization of at least one fluorinated monomer.

 $\hspace{1.5cm} \text{The process of the invention is based on two} \\ \hspace{1.5cm} \text{stages comprising}$ 

- a) the emulsification of a mixture of monomers comprising;
- 25 from 20 to 99.9% by weight of at least one monomer chosen from fluorinated (meth)acrylic monomers (A),

from 0 to 65% by weight of at least one monomer chosen from nonfluorinated (meth)acrylic or vinyl monomers (B),

from 0.1 to 15% by weight of at least one 5 polar monomer (C),

using energetic emulsifying means, such as ultrasound, colloid mill or high-pressure homogenizer, and

b) - the polymerization of the said mixture at a temperature ranging from 20 to 100°C using radical 0 initiators.

The monomers A are chosen from fluorinated (meth)acrylic monomers corresponding to the following formulae:

$$\begin{array}{c} R_{1} \\ R_{F}-(cH_{2})_{p}-so_{2}-N-(cH_{2})_{q}-o-c-c-c=cH_{2} \\ 0 \\ R_{F}-so_{2}-N-(cH_{2})_{q}-o-c-c=cH_{2} \\ 0 \\ 0 \\ R_{F}-(cH_{2})_{p}-o-c-c=cH_{2} \\ 0 \\ \end{array}$$

in which R<sub>F</sub> represents a perfluorinated radical with a linear or branched chain comprising 2 to 20 carbon atoms, p and q, which are identical or different, each 20 represent an integer ranging from 1 to 20 and preferably from 1 to 4, R<sub>1</sub> represents a linear or branched alkyl radical comprising from 1 to 4 carbon atoms and  $R_2$  represents a hydrogen atom or a methyl radical.

The nonfluorinated monomers (B) are generally alkyl acrylates or methacrylates, such as, for example, butyl methacrylate, 2-ethylhexyl methacrylate and stearyl and behenyl acrylates and methacrylates, acrylates and methacrylates carrying an oxyethylenated linkage, such as ethyl triglycol methacrylate, or vinyl monomers, such as vinyl chloride, vinylidene chloride or vinyl acetate.

Mention may be made, among the polar monomers

(C), of N,N-dimethylaminoethyl or N-tert-butylaminoethyl methacrylates and acrylates and their quaternized
derivatives, acrylic and methacrylic acids, or monomers

carrying a sulphonic acid or hydroxyl group, such as
hydroxyethyl or hydroxypropyl acrylates and
methacrylates.

Crosslinking agents are generally used to
attach the copolymer to the substrate and to render it
20 insoluble in solvents. They are acrylamide derivatives,
such as N-methylolacrylamide and N-methylolmethacrylamide, or chlorohydroxypropyl acrylate or methacrylate.

The surfactants used are anionic or cationic surfactants, such as sulphosuccinate and quaternary

ammonium derivatives, for example sodium bis(tridecyl)sulphosuccinate.

They are optionally used in combination with nonionic surfactants.

The molecular masses are adjusted using chain-transfer agents, such as mercaptans, or by the technique for introduction of the monomers. The copolymerization can be initiated at between 20 and 140°C by means of water-soluble or organosoluble initiators of peroxide type (such as hydrogen peroxide), persalt type (such as persulphates) or azo type, such as 4,4'-azobis(4-cyanopentanoic acid) or azobis(amidinopropane) hydrochloride or azobisisobutyronitrile.

The polymerization is preceded by a stage of emulsification of the mixture comprising the monomers,

15 the water and the surfactants. It is important to carry out this emulsification by energetic emulsifying means, such as ultrasound or homogenizers of the Manton-Gaulin type or a colloidal mill. The mechanical energy contributed by these devices makes it possible to shear

20 the mixture and to form fine monomer droplets stabilized by the surfactant. These fine droplets of monomers are sites of polymerization generating polymer particles with comparable sizes (50-500 nm).

The emulsions of fluorinated polymers

25 according to the invention can be used in the
hydrophobic and oleophobic treatment of a great variety
of substrates, such as textiles, leather, paper or

construction materials. They can be applied, after dilution in water, by padding, steeping, coating or spraying. They can be formulated with various additives, such as fixing resins, catalysts, antistatic agents, antifoaming agents or fungicides.

The following examples illustrate the invention without limiting it. Except when otherwise indicated, the parts and percentages are expressed by weight.

10 Example 1

### a) preparation of the latex

The following are introduced into a 1000 parts by volume reactor which is heated by a thermostatically controlled jacket and is equipped with an anchor stirrer and a reflux condenser.

- 480 parts of demineralized water
- 0.12 part of borax (Na<sub>2</sub>B<sub>2</sub>O<sub>5</sub>)
- 3.99 parts of sodium bis(tridecyl)sulpho-

succinate

20 - 8.34 parts of a mixture of polyfluorinated acrylates of formula:

$$c_{n}^{F_{2n+1}} - c_{2}^{H_{4}} - o - c - cH = cH_{2}$$

where n is equal to 8, 10, 12 and 14 in respective ratios by weight of 63:25:10:2.

25 The mixture is brought to 65°C with stirring for 30 minutes and then subjected to ultrasound (Branson Sonifier) for one minute. The following are added with stirring to this mixture which has been subjected to ultrasound:

- 58.6 parts of 2-ethylhexyl methacrylate
- 0.36 part of methacrylic acid
- 1.26 parts of N-methylolacrylamide
- 59.8 parts of a mixture of polyfluorinated

acrylates of formula:

5

$$c_n F_{2n+1} - c_2 H_4 - o - c - c H = cH_2$$

where n is equal to 8, 10, 12 and 14 in respective 10 ratios by weight of 63:25:10:2.

This mixture is subjected to ultrasound (Branson Sonifier) for one minute and then homogenized with a high-pressure homogenizer (Microfluidizer), 6 passes being carried out at 60°C.

The miniemulsion thus obtained is composed of fine droplets of monomers having a mean particle diameter of the order of 100-200 nm. It is transferred into a 1000 parts by volume reactor which is heated by a thermostatically controlled jacket and is equipped with an anchor stirrer and a reflux condenser. This miniemulsion is brought to 88°C while purging with nitrogen and the polymerization is initiated with 0.84 g of potassium persulphate dissolved in 7 g of water. An equivalent amount of initiator solution is run continuously into the reactor for one hour. The polymerization is continued for an additional hour. The

nitrogen purging is maintained throughout the duration of the polymerization.

A coagulum-free perfluorinated copolymer latex is obtained, which copolymer has the following 5 composition by mass: 53.4% of perfluorinated units, 45.8% of 2-ethylhexyl methacrylate, 0.3% of methacrylic acid and 0.47% of N-methylolacrylamide. The solids content is 20% and the mean particle diameter is 130 nm.

### b) Application to leather

The perfluorinated copolymer latex obtained is diluted in water at ambient temperature until an aqueous solution is obtained comprising 1% of active materials.

This solution is subsequently sprayed crosswise onto leather samples using a Volumair T 21 sprayer.

The amount deposited is on average 130 g/m². After drying for 24 hours at ambient temperature, the leather samples are evaluated in the following way:

### Oleophobicity tests

The oleophobicity is measured according to
the test described in "AATCC Technical Manual", test
method 118 (1992), which evaluates the non-wettability
25 of the substrate by a series of oily liquids of
decreasing surface tensions. The grading of the treated
substrate is defined as the maximum value of the test

liquid which does not wet the substrate. The test liquids employed in the evaluation are listed in the following table:

| Grading     | Test liquids for measuring | Surface tension |  |
|-------------|----------------------------|-----------------|--|
|             | the oleophobicity          | at 25°C (mN/m)  |  |
| 1           | Nujol                      | 31.5            |  |
| 2           | Nujol/n-hexadecane         | 29.6            |  |
|             | (65/35 by volume)          |                 |  |
| 3           | n-hexadecane               | 27.3            |  |
| 4           | n-tetradecane              | 26.4            |  |
| 5           | n-dodecane                 | 24.7            |  |
| 6           | n-decane                   | 23.5            |  |
| 7           | n-octane                   | 21.4            |  |
| 8 n-heptane |                            | 19.8            |  |

5

### Hydrophobicity tests

The hydrophobic effect is measured using test solutions numbered 1 to 10 and composed of water/isopropanol (IPA) mixtures in the following 10 proportions by weight:

| Test solutions | Water | Isopropanol  |
|----------------|-------|--------------|
| Tebe borderons | Macer | ISOPIOPATIOI |
| 1              | 90    | 10           |
| 2              | 80    | 20           |
| 3              | 70    | 30           |
| 4              | 60    | 40           |
| 5              | 50    | 50           |
| 6              | 40    | 60           |
| 7              | 30    | 70           |
| 8              | 20    | 80           |
| 9              | 10    | 90           |
| 10             | 0     | 100          |

These tests consist in depositing drops of these mixtures on the treated substrates and in then observing the effect produced. The grading is carried out by giving, as the value, the number corresponding to the solution which has not penetrated or wetted the substrate after being in contact for 30 seconds.

In this example, the treated leather samples

10 are lamb skin. The results of this treatment are
recorded in the table below:

|           | AATCC 118 | Water/IPA |
|-----------|-----------|-----------|
| Treated   | 4         | 5         |
| Untreated | 0         | 0         |

This table shows the notable effectiveness of this product.

### Example 2

### a) preparation of the latex

- The following are introduced into a 1000 parts by volume reactor which is heated by a thermostatically controlled jacket and is equipped with an anchor stirrer and a reflux condenser:
  - 480 parts of demineralized water
  - 0.12 part of borax (Na<sub>2</sub>B<sub>2</sub>O<sub>5</sub>)
  - 3.99 parts of sodium bis(tridecyl)sulpho-

succinate

 8.34 parts of a mixture of polyfluorinated acrylates of formula:

$$C_n F_{2n+1} - C_2 H_4 - O - C - CH = CH_2$$

15

25

5

10

where n is equal to 8, 10, 12 and 14 in respective ratios by weight of 63:25:10:2.

The mixture is brought to 65°C with stirring for 30 minutes and then subjected to ultrasound

- 20 (Branson Sonifier) for one minute. The following are added with stirring to this mixture which has been subjected to ultrasound:
  - 28.58 parts of 2-ethylhexyl methacrylate
  - 0.27 part of methacrylic acid
  - 0.95 part of N-methylolacrylamide
  - 90.2 parts of a mixture of polyfluorinated acrylates of formula:

$$c_n r_{2n+1} - c_2 H_4 - o - c - c H = c H_2$$

where n is equal to 8, 10, 12 and 14 in respective ratios by weight of 63:25:10:2.

This mixture is subjected to ultrasound (Branson Sonifier) for one minute and then homogenized with a high-pressure homogenizer (Microfluidizer), 6 passes being carried out at 60°C.

The miniemulsion thus obtained is composed of fine droplets of monomers having a mean particle

10 diameter of the order of 100-200 nm. It is transferred into a 1000 parts by volume reactor which is heated by a thermostatically controlled jacket and is equipped with an anchor stirrer and a reflux condenser. This miniemulsion is brought to 88°C while purging with

15 nitrogen and the polymerization is initiated with 0.84 g of potassium persulphate dissolved in 7 g of water. An equivalent amount of initiator solution is run continuously into the reactor for one hour. The polymerization is continued for an additional hour. The nitrogen purging is maintained throughout the duration of the polymerization.

A coagulum-free perfluorinated copolymer
latex is obtained, which copolymer has the following
composition by mass: 77.1% of perfluorinated units,

25 22.4% of 2-ethylhexyl methacrylate, 0.2% of methacrylic
acid and 0.4% of N-methylolacrylamide. The solids

content is 20% and the mean particle diameter is 120 nm.

### b) Application to leather

With the conditions described in Example 1

5 being repeated, the results obtained for Example 2 are expressed in the following table:

|           | AATCC 118 | Water/IPA |
|-----------|-----------|-----------|
| Treated   | 4         | 4         |
| Untreated | 0         | 0         |

### Example 3

10

### a) Preparation of the latex

The following are introduced into a 1000 parts by volume reactor which is heated by a thermostatically controlled jacket and is equipped with an anchor stirrer and a reflux condenser:

15

- 670 parts of demineralized water
- 13 parts of dicocodimethylammonium

chloride

- 12 parts of a mixture of ethoxylated alkylphenol with an HLB of 15
- 20 200 parts of a mixture of polyfluorinated acrylates of formula:

$$C_n F_{2n+1} C_2 H_4 OC - CH = CH_2$$

where n is equal to 8, 10, 12 and 14 in respective ratios by weight of 63:25:10:2

- 65 parts of stearyl methacrylate
- 8.5 parts of N-methylolacrylamide as a 48% solution in water
- 9.2 parts of N-methylolmethacrylamide as a 5 60% solution in water
  - 0.27 part of n-dodecyl mercaptan.

This mixture is brought to 65°C without stirring for 30 minutes, then subjected to ultrasound (Branson Sonifier) for one minute, then homogenized with a high-pressure homogenizer (Microfluidizer), 6 passes being carried out at 60°C.

The miniemulsion thus obtained is composed of fine droplets of monomers having a mean diameter of the order of 150-200 nm. It is transferred into a 1000

15 parts by volume reactor which is heated by a thermostatically controlled jacket and is equipped with an anchor stirrer and a reflux condenser. This miniemulsion is brought to 70°C while purging with nitrogen and the polymerization is initiated with 2.03

20 parts of azobisisobutyronitrile dissolved in 20 parts of water. The polymerization takes place in two hours.

After cooling, a coagulum-free perfluorinated copolymer latex is obtained, which copolymer has the following composition by mass: 70.7% of perfluorinated units, 23% of stearyl methacrylate, 3% of N-methylolacrylamide and 3.3% of N-methylolmethacrylamide. The solids content is 33% and is brought to 20% by diluting

with water. The mean diameter of the particles is 150 nm.

### b) Application to textiles

A padding bath comprising 25 g/l of the

5 fluorinated copolymer latex obtained above and 1.5 g/l
of acetic acid in water is prepared at ambient
temperature. The fabrics are subsequently padded in
this bath with a degree of expression of the order of
50%. After drying, the fabrics are treated for one

10 minute at 160°C in a Benz thermal curing device.

The fabrics thus treated are subsequently tested with regard to oleophobicity and hydrophobicity. The oleophobicity is tested according to the AATCC 118 test described above. The hydrophobicity is evaluated according to a test of resistance to wetting by water used to monitor the water-repellent finishing of the fabric (Spray Test according to AATCC Technical Manual, Test Method 22, 1972).

A polyamide (PA) fabric was treated.

20 The highly advantageous performance of this product is shown in the table below.

|    | AATCC 118 | Spray Test |
|----|-----------|------------|
| PA | 6         | 100        |

### CLAIMS

- Process for producing fluorinated polymers by miniemulsion polymerization in two stages
   comprising
  - a) the emulsification of a mixture of monomers comprising:

from 20 to 99.9% by weight of at least one monomer chosen from fluorinated (meth)acrylic monomers 10 (A).

from 0.1 to 15% by weight of at least one monomer chosen from acrylamide and its derivatives, such as N-methylolacrylamide, and

from 0 to 65% by weight of at least one
15 monomer chosen from nonfluorinated acrylic or vinyl
monomers (B),

using energetic emulsifying means, such as ultrasound, colloid mill or high-pressure homogenizer, and

20 b) the polymerization of the said mixture at a temperature ranging from 20 to 100°C using radical initiators.

the level of organic cosolvent being less than 0.2% by weight of the total weight of the 25 emulsion.

2. Process according to Claim 1, characterized in that the mixture of monomers is

stabilized by at least one surfactant chosen from the group comprising nonionic, anionic or cationic surfactants, such as polyethoxylated sulphosuccinate derivatives or quaternary ammonium derivatives.

3. Process according to Claim 1 or 2, characterized in that the fluorinated monomer A is chosen from the group comprising the monomers corresponding to the following formulae:

in which R<sub>F</sub> represents a perfluorinated radical with a linear or branched chain comprising 2 to 20 carbon

15 atoms, p and q, which are identical or different, each represent an integer ranging from 1 to 20 and preferably from 1 to 4, R<sub>1</sub> represents a linear or branched alkyl radical comprising from 1 to 4 carbon atoms and R<sub>2</sub> represents a hydrogen atom or a methyl

20 radical.

- 4. Process according to one of the preceding claims, characterized in that the monomer B is chosen from the group comprising:
  - C1-C22 alkyl (meth)acrylates
- 5 (meth) acrylates, the radical of which carries an oxyethylenated linkage
  - vinyl monomers, such as vinyl chloride or vinyl acetate
    - acrylic and methacrylic acids.
- 5. Process according to one of the preceding claims, characterized in that the initiator is chosen from the group comprising:
  - peroxides
  - persalts, such as persulphates
- azo compounds, such as 4,4'-azobis
  (4-cyanopentanoic acid).
- 6. Aqueous dispersion of fluorinated polymers as may be obtained according to the process of any one of the preceding claims, the content of organic cosolvent of which is less than 0.2% by weight of the total weight of the emulsion and the level of coagulum being less than 1% by weight of the total weight of
- Application of the aqueous dispersion of
   Claim 6 in the hydrophobic and oleophobic treatment of various substrates, such as leather, textiles, fitted carpets, paper and construction materials.

### ABSTRACT

\* \* \* \* \*

# FLUORINATED POLYMERS BY MINIEMULSION POLYMERIZATION

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Inventors:

Mr Denis TEMBOU NZUDIE

Mr Didier JUHUE

Mr Jean-Marc CORPART

....

The invention discloses a process for the preparation of fluorinated polymers by miniemulsion polymerization of a mixture of fluorinated and nonfluorinated monomers in the absence of organic solvent.

This polymerization process makes it possible to obtain an aqueous emulsion of fluorinated polymers devoid of coagulum.

33808F147

### Declaration and Power of Attorney United States Patent Application

UNITED STATES Patents and Design Patents Sole & Joint Inventors Convention & Non-convention PCT & Non-PCT This form cannot be amended, altered or changed after it is signed. (For use only for inventors who

As a below named inventor, I hereby declare that:

| I believe I am th                                      | he original, first and sole in   | zenship are as stated below next to my nam<br>wentor (if only one name is listed below) o<br>) of the subject matter which is claimed an  | or an original, first and joint  | understand the English language.)  |
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|  |  | nts of the above-identified specification, in<br>ation which is material to patentability as  |  |  |
| certificate, or §<br>have also ident                   | 365(a) of any PCT interna  | der Title 35, United States Code, §119(a)-<br>tional application which designated at leas<br>plication for patent or inventor's certificate<br>d:   | t one country other than the United States   | of America listed in this Declaration. 1   |
| Foreign/l  | PCT Application No.  | Country   | Filing Date  | Priority Claimed? (yes/no)   |
| 98/14272   |  | France  | 11/13/98   | YES  |
| United States of<br>application or I<br>information wh | of America listed in this De<br>PCT international application<br>inich is material to patentab | United States Code, §120 or §365(e) of arctelaration and, insofar as the subject matter ion in the manner provided by the first parality as defined in Title 37, Code of Federa national filing date of this application: | of each of the claims of this application in<br>agraph of Title 35, United States Code, §1 | s not disclosed in the prior United States<br>12, I acknowledge the duty to disclose |
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| Weilacher (20.   | 531), Herbert M. Hanegan<br>is C. Rodgers (32,936), W  | o prosecute this application and to transac<br>(25,682), Dale Lischer (28,438), Frederic<br>filiam F. Rauchholz (34,701), Michael K.  | k F. Calvetti (28,557), J. Rodgers Lunsfor   | d, III (29,405), Michael A. Makuch   |
|  | pondence to: SMITH, GAI<br>ect all phone calls to (202)  | MBRELL & RUSSELL, LLP, 1850 M Stre<br>0 659-2811.   | et, N.W. (Suite 800), Washington, D.C. 20  | 0036. All facsimiles may be sent to (202)  |
| be true; and fu<br>both, under Se                      | rther that these statements  | herein of my own knowledge are true and<br>were made with the knowledge that willful<br>the United States Code and that such willful<br>on.   | I false statements and the like so made are  | punishable by fine or imprisonment, or   |
|  |  | r: Dennis Tembou Nzudie<br>Serquigny, France 70,<br>70, parc Maubuisson, F-27470<br>Serquigny, France   |  | Citizenship: FRANCE  |
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| Post office Signature:                                 | (city, state, country): address:   | or, if any: Didier Juhne  Levallois-Perret Fran  89ter, ruc Edouard Va Levaliois-Perret, Fran  atjons are listed in attached Supplemental   | Date: 6/21/01  | Citizenship: FRANCE<br>nee_ Citizenship: FRANCE<br>La Fontaine<br>Gernon             |

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